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Rc:

Exhaust Gas Purifying Catalyst And Process For Purification Of

Exhaust Gas

Applicant:

Takeshi Matsumoto

Application No.:

10/535,331 5/18/2005

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Attached please find the executed Declaration.

Please do not hesitate to contact me with any questions.

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IN THE UNITED STATES PATENT AND TRADEMARK OFFICE

In re Patent Application of TAKESHI MATSUMOTO ET AL

5 Serial No. 10/535,331

Group Art Unit: 1755

Filed: May 18, 2005

Examiner: Wood, Elizabeth D

Title: EXHAUST GAS PURIFYING CATALYST AND PROCESS FOR

PURIFYING OF EXHAUST OF GAS

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DECLARATION

UNDER 37 C.F.R. 1.132

- I, Takuji Nakane, a citizen of Japan, residing at 344-1-706, Waku, Aboshi-ku, Himeji-shi, Hyogo-ken, Japan, declare:
 - I. I am one of co-inventors in the above referenced application, and a chemist as well as a Researcher of AC Research Laboratory of ICT CO., LTD., one of co-assignees of this application, on the subject matters relating to this application.

I graduated from Tokyo Institute of Technology, Faculty of Science, Department of Chemistry in March 1997 and Graduate School of Tokyo Institute of Technology, Department of Chemistry in March 1999, and obtained a master degree majoring surface science.

Since April, 1999, I have been the employee of ICT CO., LTD. at AC Research Laboratory and have been engaged in the research work with respect to catalysts for purifying exhaust 30 gas of diesel engine.

I am well acquainted with all the other co-inventors in this case, having worked with them on the development of

the invention described in this application.

II. In order to compare the effects of the catalysts of this application with those catalysts of Labarge et al I (US 5 6,489,259) and Labarge et al II (US 2002/0086793), I have conducted the following experiments:

Example 8

A catalyst was prepared by a similar method to Example 4 of this application. During the test for performance of purifying exhaust gas, light oil containing 0.03% by weight of sulfur was used as a fuel for an internal combustion engine. The results were summarized in Table 1A.

15			TA	BLE 1A			
Inlet temp.	нC	CO	NOx	02	· CO ₂	SO₂	L.Q.
of catalyst	(ppm)	(ppm)	(ppm)	(vol.%)	(vol.%)	(ppm)	(mL/min)
layer							
500°C	30	90	380	6.5	10.2	12	8.5
450°C	45	100	360	8.1	9.1		7.0
400°C	50	110	320	9.6	8.0	-	6.5
350°C	60	120	240	11.0	7.0	-	5.5

L.O.: Light oil

Comparative Example 3

A similar method to Example 4 of this application was carried out except that ZSM-5 having 2-4 µm of particle diameter was used. Test results of Comparative Example 3 and Example 8 were summarized in Table 5.

TABLE 5 Initial NOx purification activity (%)

	500°C	450°C	400°C	350°C
Example 8	4.5	42	43	23
Comparative	35	35	37	22
Example 3				·

Example 9

Catalyst was prepared by a similar method to Example 4 of this application except that 116g of ZSM-5, 91g of β-zeolite, 42g of Copper nitrate and 42g of silica sol were used. In this case, weight ratio of ZSM-5 and β-zeolite was 11:8. During the test for performance of purifying exhaust gas, light oil containing 0.003% by weight of sulfur as a fuel for an internal combustion engine. The results were summarized in Table 1B.

TA	BI	E	1	В
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			1.73	DDC ID			
Inlet temp.	HC (ppm)	CO (ppm)	NOx (mqq)	O ₂ (vol.%)	CO ₂	50 ₂	L.O.
layer							
500°C	200	170	330	6.5	10.2	15	8.5
450°C	160	160	300	8.1	9.1	_	7.0
400°C	140	180	250	9.6	B.O	_	6.5
350℃	180	240	200	11.0	7.0	_	5.5

L.O.: Light oil

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Example 10

A similar method to Example 9 described above was carried out except that 160g of ZSM-5 and 43g of β -zeolite were used. In this case, weight ratio of ZSM-5 and β -zeolite was 5:1.

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Comparative Example 4

Acatalyst was prepared by a similar method to Comparative Example 1, and a similar purification test was carried out.

The results of the test were shown in Table 2A including those of Examples 9 and 10 and Comparative Example 4.

			TABLE 2A		
	Ono —	SSM5 (MFI	2SM5 (MFI zeolite)	BEA (\$ zeolite)	/2-MSZ
-					ß-zeolite
		SiO ₂ /Sl ₂ O ₃ =70	SiO ₂ /3l ₂ O ₃ =30	\$102/\$1 ₂ 0 ₃ =25	
_					
	-	Average Crystal:	Average Crystal:		
		less than 0.05 µm	0.4 um		
Example 9	7	7.			
		25		40	11:8
Example 10	7	76		19	5.1
Comparative	7	95			1.5
Example 4					>
!!					•

In Table 2: Unit: 9/ litter catalyst

TABLE 6 Initial NOx purification activity (%)

	500°C	450°C	400°C	350°C
Example 9	44	45	44	33 .
Example 10	43	45	47	39
Comparative	42	. 46	47	28
Example 4				

TABLE 7 NOx purification activity (%) after durability test

	500°C	450°C	400°C	350°C
Example 9	42	43	41	20
Example 10	44	42	40	23
Comparative	13	39	40	• 15
Example 4				

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III. CONCLUSION

According to Table 5, a catalyst of this invention (i.e., the catalyst of Example 8), in which ZSM-5 had an average particle diameter not greater than 0.5 µm, was more active in reducing NOx in exhaust gas than a comparative catalyst (i.e., the catalyst of Comparative Example 3), in which ZSM-5 had an average particle diameter greater than 0.5 µm.

According Tables 6 and 7, a catalyst of this invention (i.e., the catalyst of Example 9 or 10), in which the weight ratio of ZSM-5 to β zeolite falled within the range of 1:0.1 to 1:5 recited in claim 1, was more active in reducing NOx in exhaust gas at low inlet temperature, i.e., 350°C, than a comparative catalyst (i.e., the catalyst of Comparative Example 4), which, like LaBarge's catalyst, contained ZSM-5, but not β zeolite.

The undersigned Takuji Nakane declare that all the statements made herein are true; and further that these statements are made with the knowledge that willful false statements and the like so made are punishable by fine or imprisonment, or both under Section 1001 of Title 18 of the United States Code and that such willful false statements may jeopardize the validity of the application or any patent issuing thereon.

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Dated this 18th day of February, 2008.

By Takuji Nakane
Takuji Nakane

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